

portant potential applicability: reactions which because of steric hindrance between adsorbate and surface would be expected to occur more readily at projecting atoms than on atoms in densely packed crystal faces and competitive reactions which would specifically illuminate structure sensitivity for strengths of binding of reactants to the surface.

Balandin and Klabunovskii have investigated the hydrogenation of some highly hindered tripticenes which they suggest can occur only at protuberances from the surface.⁴ However, for ease in purification, in chemical analysis, and in interpretation, di-*tert*-butylacetylene or *trans*-di-*tert*-butylethylene appears more attractive. They have been hydrogenated.^{5,6} Models indicate that the adsorbed species of the conventional mechanism of hydrogenation would involve substantial steric interaction between the *tert*-butyl groups and densely packed surfaces like (100) and (111) of fcc, but that there would be much less steric hindrance at steps or edges. We are examining these reactions alone and competitively and we have started with supported platinum catalysts of various degrees of dispersion.

We have assumed that cyclopentene and diethylacetylene adsorb with little or no steric hindrance and we have used them as reference compounds in rate comparisons and in competitive hydrogenations. Reactions were run in a miniature liquid-phase batch reactor of the Hussey⁷ type with the Hussey technique of successive injections in which runs are sandwiched between two runs of a reference substance, in our case, cyclopentene. No runs were accepted unless both cyclopentene runs were strictly zero order and of the proper rate. Very careful purification of reactants and attention to detail is needed to avoid poisoning. Our experiences have led us to doubt the validity of rate measurement in any liquid-phase hydrogenation not using similar controls. In our experiments about 0.1 cm³ of acetylene or olefin, 1 cm³ of solvent (cyclohexane), 10–30 mg of catalyst, and a total pressure of 1 atm were employed.

Pt/SiO₂ catalysts were prepared by ion exchange of Pt(NH₃)₄²⁺ with 200+ mesh large pore Davison silica gel, grade 59, following the recipes of Dorling, Lynch, and Moss.⁸ The 0.5% Pt/SiO₂ was reduced in hydrogen at 300°; the 1.9% Pt/SiO₂ was additionally sintered in air at 450° before reduction. Dispersions were measured by hydrogen chemisorption (Table I) and the results were in good agreement with ref 8. The 1% Pt/Al₂O₃ was prepared by impregnation of 200+ mesh η-Al₂O₃⁷ with diamminoplatinum dinitrite⁷ followed by heating in oxygen at 500°, cooling in nitrogen to 350°, and reduction at that temperature by hydrogen. Pt/Al₂O₃ (1.1%), prepared similarly from γ-Al₂O₃ (Catapal, Continental Oil Co.), was reduced at 780°. Dispersions are given in Table I.

The course of hydrogenation of di-*tert*-butylacetylene was determined by removal and gas chromatographic analysis of samples. Both Pt/SiO₂ catalysts gave initial

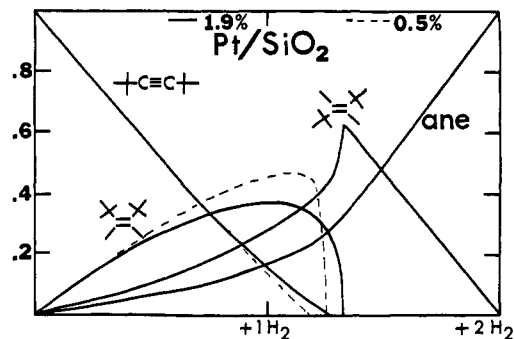


Figure 1. Hydrogenation of di-*tert*-butylacetylene: *x* axis, moles of H₂ added; *y* axis, hydrocarbon fraction.

Table I. Hydrogenations, Separate and Competitive at 20°

Catalyst	% dispersion	<i>S</i> _{5/10} ^a	<i>k</i> ₅ ^b	<i>k</i> ₁₀ / <i>k</i> ₅ ^c
0.5% Pt/SiO ₂	54	90	15	0.68
1.9% Pt/SiO ₂	14	240	12	0.78
1.0% Pt/η-Al ₂ O ₃	100	60	2.7	0.36
1.1% Pt/γ-Al ₂ O ₃	31	140	7.3	0.85

^a The selectivity for hydrogenation of cyclopentene *vs.* di-*tert*-butylacetylene in competitive experiments. We list the initial value of $(\ln(C_5^\circ/C_5)/\ln(C_{10}^\circ/C_{10}))$. ^b Turnover number in molecules of cyclopentene hydrogenated per second per surface Pt at a hydrogen pressure of 1 atm. ^c Ratio of initial rate of hydrogenation of the acetylene alone to that of cyclopentene alone.

selectivities for *cis*-di-*tert*-butylethylene of 66%, for the *trans* ene of 21%, and for di-*tert*-butylethane of 13%. The more highly dispersed Pt/Al₂O₃ gave 80, 17, and 5%, the less highly, 77, 14, and 9%. As shown in Figure 1, further reaction of *cis* ene on Pt/SiO₂ is not completely inhibited by the acetylene but the degree of inhibition is much greater on the more highly dispersed Pt/SiO₂. Results on Pt/Al₂O₃ had the same general form and, in particular, the same effect of the degree of dispersion was noted. Isomerization of *cis* ene to *trans* ene is faster than its hydrogenation to ane, a situation unusual on platinum.⁷ Hydrogenation of the *trans* ene is slow relative to that of the acetylene.

The table shows rates of hydrogenation of cyclopentene and di-*tert*-butylacetylene singly and the selectivity ratio when the two are hydrogenated competitively. The rate of hydrogenation of the acetylene alone is not much less than that of cyclopentene but, competitively, the acetylene reacts very much more slowly. In competitive hydrogenations, the initial overall rates were very near those of cyclopentene alone. On the Pt/η-Al₂O₃, the rate ratio *k*₆/*k*₁₀ for diethylacetylene *vs.* di-*tert*-butylacetylene is 1.15 and the selectivity ratio *S*_{5/6} is 0.14. Thus, although the two acetylenes hydrogenate at about the same rate, *S*_{6/10} would be 430 in competitive runs with the two assuming⁷ that *S*_{6/10} = *S*_{5/10}/*S*_{5/6}.

The turnover numbers for hydrogenation of cyclopentene and the acetylene do not vary greatly among the catalysts but the numbers are lower on Pt/Al₂O₃ than on Pt/SiO₂ particularly on the highly dispersed Pt/Al₂O₃. The reactions are clearly structure sensitive, but the effect of structure sensitivity appears less in overall rates than in selectivity factors, in variation from catalyst to catalyst of the strength or rate of adsorption of the acetylene *vs.* *cis* ene and *vs.* cyclopentene. On the cata-

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(6) R. B. Turner, D. E. Nettleton, Jr. and M. Perelman, *J. Amer. Chem. Soc.*, **80**, 1430 (1958).

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(8) T. A. Dorling, B. W. J. Lynch, and R. L. Moss, *J. Catal.*, **20**, 190 (1971).

lysts reported here, the more highly hindered reactant, di-*tert*-butylacetylene, is a better competitor *vs.* cyclopentene and the *cis* ene on the catalyst of highest dispersion, that is, on the catalysts in which there is presumably a higher proportion of projecting platinum atoms. However, it appears that other factors are also involved.

Transport of hydrogen between gas and solution is not limiting in our experiments nor are there serious concentration gradients in the pores of the catalysts. We examined the more highly dispersed Pt/SiO₂ in mesh sizes 120–140, 200–270, and 400+. The selectivity ratio $S_{3/10}$ was the same for all; k_3 was somewhat smaller for mesh 120–140 but equal for the other two.

More platinum catalysts must be examined before firm conclusions can be drawn but clearly the reactions in question and competitive reactions in general will be useful in studying structure sensitivity.⁹

Acknowledgment is made to the donors of the Petroleum Research Fund, administered by the American Chemical Society, for support of this work.

(9) We will be happy to furnish those interested in using these reactions with descriptions of methods which we have found to be satisfactory for purification and oxygen-free storage of solvents and reactants.

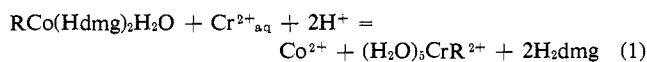
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Alkyl Transfer from Cobalt to Chromium¹

Sir:

A subject of some current interest is the cleavage of the Co–C σ bond in organo-aquacobaloximes² including reactions in which the alkyl group R is transferred to another metal.^{3–12} Several mechanisms must be invoked to explain these observations, because the alkyl group in such reactions may be transferred (in a formal sense at least) as a carbanion, as a radical, and as a carbonium ion.

We wish to report that organocobaloximes react with Cr²⁺_{aq} with essentially quantitative transfer of the alkyl group to chromium (eq 1). The Cr(III) product



(1) Work performed in the Ames Laboratory-USAEC with partial support from the National Science Foundation.

(2) Cobaloxime is the trivial name for the bis(dimethylglyoximate) complexes of cobalt.

(3) A. Adin and J. H. Espenson, *Chem. Commun.*, 653 (1971).

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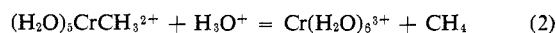
(10) H. A. O. Hill, J. M. Pratt, S. Risdale, F. R. Williams, and R. J. Williams, *Chem. Commun.*, 341 (1970).

(11) F. R. Jensen, V. Madan, and D. H. Buchanan, *J. Amer. Chem. Soc.*, **93**, 5283 (1971).

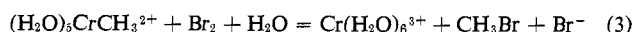
(12) G. N. Schrauzer, J. H. Weber, T. M. Beckham, and R. K. Y. Ho, *Tetrahedron Lett.*, 275 (1971).

is (H₂O)₅CrR²⁺, of which the methyl complex was the only previously known simple alkyl derivative.^{13,14}

The product in the case of the methyl derivative can be isolated from the reaction solutions at low [H⁺] in *ca.* 60% yield using ion-exchange chromatography (Dowex 50W-X2, Li⁺ form, elution with 0.35 *F* LiClO₄). The actual yields are much higher—at least 80% (H₂O)₅CrCH₃²⁺ based upon spectral analysis of the product solutions—but considerable quantities are lost to acid hydrolysis (eq 2) during the ion-exchange isolation.



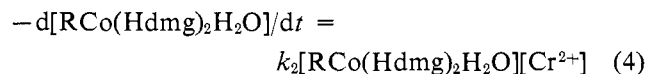
The identity of the methylchromium complex was established by comparison of the visible–uv spectrum¹⁵ and the rate and products of the acid hydrolysis reaction with that of the authentic complex.^{13,14} Also, methane was the only volatile product of acid hydrolysis which could be detected mass spectroscopically, and methyl bromide the only volatile product detected upon reaction of the product with Br_{2(aq)} (eq 3). The rate constants of



these reactions agree with the values determined on authentic samples of (H₂O)₅CrCH₃²⁺.^{16,17}

The reactions have also been studied for R = CH₂CH₃, *n*-C₃H₇, CH₂C₆H₅, CH₂C(CH₃)₃, CH(CH₃)₂, and 2-octyl. Ion exchange isolation of the organochromium product was successful for the first three compounds but has not been attempted for the neopentyl and 2-octyl derivatives. The isopropylchromium(III) ion hydrolyzes rapidly enough so that the complex could not be isolated in this manner.

The reactions were studied at 25° in aqueous perchloric acid solutions having an ionic strength of 1.0 *M*. The reaction follows a second-order rate expression (eq 4), the rate constant for both the neutral and protonated



forms of the cobaloxime being determined from the dependence of the apparent second-order rate constant upon [H⁺], which was consistent with the known protonation constants of the coordinated oxime function.³

The kinetic data are in accord with the mechanism shown in Scheme I, and were fit to this mechanism using the independently determined values of the protonation

(13) (a) W. Schmidt, J. H. Swinehart, and H. Taube, *J. Amer. Chem. Soc.*, **93**, 1117 (1971); (b) M. Ardon, K. Woolmington, and A. Pernick, *Inorg. Chem.*, **10**, 2812 (1971).

(14) Although R = CH₃ was the only simple alkyl derivative known, various other organochromium compounds of this formula have been prepared including the benzyl [J. K. Kochi and D. B. Buchanan, *J. Amer. Chem. Soc.*, **87**, 859 (1965)], various haloalkyls [F. A. L. Anet, *Can. J. Chem.*, **37**, 58 (1959); D. Dodd and M. D. Johnson, *J. Chem. Soc. A*, **34** (1968)], and other substituted alkyls.^{13a}

(15) The Cr(III) product had the following uv–visible spectrum, given as λ_{max} , nm (ϵ , M⁻¹ cm⁻¹): 530 (15.7), 392 (240), and 158 (2510) in comparison with the literature values 550 (9.6), 392 (196), and 258 (2160). However, the latter values were determined by Ardon, *et al.*,¹⁴ on a sample eluted with 0.35 *F* HClO₄ such that partial decomposition according to eq 3 was inevitable, leading to low values of ϵ . On repeating this preparation using LiClO₄ as the eluting agent, the spectrum of (H₂O)₅CrCH₃²⁺ was 538 (11.5), 392 (246), and 258 (2400).

(16) The Cr(III) product reacted with perchloric acid according to eq 2 with a pseudo-first-order rate constant of 5.0 × 10⁻³ sec⁻¹ (25.0°, 1.00 *M* H⁺, μ = 1.09 *M*). Under the same conditions the specific rate of the authentic complex is 5.2 × 10⁻³ sec⁻¹.^{13a}

(17) The Cr(III) product and authentic (H₂O)₅CrCH₃²⁺ both react with Br_{2(aq)} according to eq 3; the second-order rate constant is 2.1 × 10⁵ M⁻¹ sec⁻¹ (25.0°, μ = 1.00 *M*): J. H. Espenson and D. A. Williams, unpublished observations.